# Catalytic Decomposition of Perfluorinated Carbons (PFCs) During the Aluminium Smelting Process

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#### Abstract



Perfluorinated carbons (PFCs) are potent greenhouse gases that are formed in the primary aluminium industry when the alumina  $(Al_2O_3)$  concentration in the reduction cell is depleted. Hydrolysis on the surface of an  $Al_2O_3$ -based catalyst is potentially a viable method of PFC breakdown with the advantage of compatibility with the current process. The waste heat within the aluminium cell itself can be used to reach reaction temperatures for the catalytic process to occur, the spent catalyst can be easily disposed by feeding to the reduction cell, and the hydrogen fluoride (HF) byproduct of the catalytic decomposition can be captured using conventional dry-scrubbing techniques.

This study takes an in-depth look at tuning the surface chemistry of the alumina-based catalyst to maintain high-efficiency of PFC breakdown in a HF-rich environment which will poison the catalyst surface over time. Maximizing Lewis acid sites on the catalyst surface is believed to be the key to optimization. Characterization methods have provided quantitative and qualitative data to determine which catalyst is best suited for PFC decomposition.

Keywords: Perfluorinated carbons, Alumina catalyst, Surface acidity, Al NEXAFS, Primary Aluminium production

#### 1. Introduction

Perfluorinated carbons (PFCs) are highly stable compounds produced as a byproduct in primary aluminium smelting when the alumina concentration in the reduction cell is depleted and voltage rise causes the decomposition of the electrolyte. PFCs are also potent greenhouse gases that absorb infrared radiation in the atmosphere where naturally occurring greenhouse gases do not. PFCs persist in the atmosphere, with lifetimes exceeding 50 000 years and have a global warming potential of at least 6500. According to the Montreal protocol, the reductions required for the stabilization of the atmospheric concentration is to stop the emission of PFCs altogether [1].

The structure of alumina has been characterised extensively due to its significance as an adsorbent and solid acid catalyst. Alumina, in particular  $\gamma$ -alumina ( $\gamma$ -Al<sub>2</sub>O<sub>3</sub>), contains tetragonally distorted (AlO<sub>4</sub>) defect spinel lattices as well as the preferred, fully occupied, octahedrally coordinated (AlO<sub>6</sub>) spinel structure. The stoichiometry of producing the appropriate ratio of Al:O in  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> cannot be accommodated by both aforementioned sublattices, which means that some spinel cation sites will be vacant and primarily exist in tetrahedral sites [2, 3]. This coordinatively unsaturated site, along with fully occupied sublattices on the surface of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, are the sites that actively participate in catalysis. Catalytic decomposition of PFCs has been demonstrated using an alumina-based catalyst [4, 5]. The proposed mechanism involves a 2-step hydrolysis process that takes places on the  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> surface. The rate determining step involves a bridging O atom, which connects two adjacent Al atoms that acts as the Lewis acid site to attack the PFC (e.g., CF<sub>4</sub>) gas to form an aluminium-fluoride and aluminium-carbocation intermediate. The two intermediates then undergo a fast reaction with H<sub>2</sub>O to form neighbouring Al-OH pairs and release CO<sub>2</sub> and HF as waste products. The second step is when Al-OH pairs then undergo a hydrolysis reaction to reform the Lewis acid site [4].

The focus of this research is to characterise the Lewis acid sites on the surface of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> as a guideline to the efficiency as a catalyst decomposing PFCs. This is done using quantitative (eg. Acid-Base Titration, BET) and qualitative (eg. NEXAFS, XRD) techniques.

### 2. Methodology

**Preparation of**  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalyst samples: Different sample precursors were utilised as follows: Bayer gibbsite precursor samples were sourced from a commercial refinery, whilst gibbsite and pseudo-boehmite precursor samples were sourced from BASF. Precursor samples were calcined to target temperatures from 400-1000°C at 2 °C min<sup>-1</sup> for 24h without quenching unless stated otherwise.

*X-Ray Diffraction (XRD) for phase analysis:* XRD is commonly used to analyse the phase composition of the Al<sub>2</sub>O<sub>3</sub>-based catalyst. The XRD pattern was obtained using a Rigaku MiniFlex<sup>TM</sup> II X-ray diffractometer with scans conducted in the 2 $\theta$  range of 10-80°, with a 0.02° step size. This research looks at the different crystalline phases present in each of the calcined samples by comparing literature XRD patterns with those attained using the specified XRD.

*Surface area pore analysis:* Preparation of sample for analysis was done using 1g of catalyst that is dried at 110 °C for 18 hours to remove surface adsorbed gas species. Pore analyses of samples were measured using a Micromeritics Tristar 3000 instrument using nitrogen for physisorption experiments at 77 K. Specific surface areas (SSAs) were determined using the Barrett-Joyner-Halenda method [6].

Acid-Base Titration: Titration was conducted by preparing 100 mL of 0.1 mol/L of n-butylamine and placing 5 g of alumina sample and mixing for 30 minutes. The mixture is then left to sit for 5 minutes then decanted. Triplicate runs are then prepared using 25 mL of the decanted solution with methyl orange that is titrated against 0.1 mol/L solution of methanesulfonic acid until the endpoint volume is obtained.

*Near-Edge X-Ray absorption fine structure (NEXAFS):* NEXAFS data was obtained on the Soft X-ray (SXR) beamline at the Australian Synchrotron, the specifications and sample preparation of which have been described elsewhere [7]. Data obtained from this experiment was processed using the QANT Igor macro (Version 7.08, 2019) developed by Gann et al. [8].

#### 3. Results and Discussion

## 3.1. Phase Composition Analysis

All XRD patterns shown are compared against Inorganic Crystal Structure Database (ICSD) data to identify which phases are most dominant at a specific calcination temperature. Figure 1 shows the XRD pattern of the Bayer gibbsite precursor. Calcined samples from 400 - 800 °C show a mixture of both  $\alpha$ -Al<sub>2</sub>O<sub>3</sub> and predominantly  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> phases. Upon calcination at 900 °C onwards

#### 4. Conclusions and Future Work

In this study we have used a range of complementary methods to determine which Al<sub>2</sub>O<sub>3</sub> based catalyst, at specified calcination temperatures, shows the highest levels of surface acidity. This gives a lead into the materials likely linked with better performance in PFC decomposition [5]. NEXAFS is a useful technique to demonstrate in which coordination acid sites are present whilst acid-base titration quantitatively shows the total acidity of the catalyst surface.

This work has provided the necessary foundations to continue screening potential catalysts that can decompose PFCs in a HF rich environment present in current industrial reduction cells. In the future, catalysts will be tested under simulated industrial environments, characterisation work to give more comprehensive data on the surface chemistry of the alumina catalyst. More complex precursors will be examined to alter the resulting surface chemistry. This will also include approaches, such as acid leaching the commercial samples to investigate the effect of soda, to provide further information on surface acidity.

#### 5. References

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