Analysis of Turbulence of Aluminium and Molten Cryolite in the Aluminium Electrolysis Cell

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Abstract

The aluminium electrolysis cell used in Hall-Héroult process contains two stratified molten materials (aluminium and cryolite). These fluids are subjected to gravity, shear and high-intensity electromagnetic stresses. The two-fluid flow is important as it ensures distribution of alumina and heat throughout the cell; avoids depletion of reactants and local overheating. However, on the other hand, it is difficult to describe the flow of fluids at any time throughout the volume of the cell. The fluids are opaque, of high temperature and excessively aggressive and the cell is of complex geometry. It is very important to define the parameters that influence the flow of both fluids. In this article, a comparison is made to test different turbulence models to simulate the fluid flow in the cell. Different approaches using the Reynolds Averaged Navier-Stokes (RANS) and using the Large Eddy simulation (LES) method are compared. A simplified model of the electrolytic cell is considered for this purpose in order to investigate the transient fluctuations of the fluids velocity field in aluminium electrolysis cell.

Keywords: Aluminium electrolysis, two-phase flow, stratified fluids, magnetohydrodynamics of aluminium electrolysis cells, turbulence models.

1. Introduction

The Hall-Héroult process consists of the dissolution of alumina in an electrolytic bath. A high intensity electric current passes through the media resulting in the production of liquid aluminium which collects to the bottom of the cell. This reaction then produces a layer of molten aluminium at the bottom of cryolite bath at a temperature of around 960 °C [1]. On an industrial scale, this process is used in large cells, which can produce several tons of aluminium per day [2]. Liquid metal in the cell as well as the electrolytic bath where the different chemical reactions take place constitute a two-fluid system, in which, in addition to the chemical reactions, a certain number of thermo-solutal and magnetohydrodynamic phenomena occur [3]. The magnetic field is produced by the main current through which the cell is fed as well as the neighboring cells and magnetized steel parts [4]. The two fluids present in the cell are conductive to the electric current. Their movement within a magnetic field causes the induction of a non-negligible electric current and thus participates in the magnetism produced in and around the cell.

Fluid-flow of the bath is essential for the dispersion and the dissolution of the alumina and the distribution of the chemical species in the bath [4]. The chemical kinetics of the reactions is also influenced by the flow. The reaction rate is increased by the flow and the mixing caused by the velocity field achieves high reaction levels. The thermal balance of the cell is also influenced by the fluid flow [5]. However, the intensity of the flow must remain in a certain range to ensure

stability of the cell. High velocity fields can alter the proper functioning in terms of safety and energy efficiency of the electrolysis process. The fluctuating instabilities of the fluids in the cell go along with the modification of the shape of the interface between the aluminium and the cryolitic bath. This deformation changes the local distance between the anodes and the surface of the aluminium layer and thus the current distribution [6]. This change in distribution will typically reduce the cells performance [7].

Controlling the flow of the fluids in the electrolysis cell is very important, although it is difficult to observe the different flow regimes during its operation. Thus, an approach is based on numerical simulations to predict the behavior of the two stratified fluids. The two fluids are subjected to a very high electrical current in the range of $\sim 400\ 000\ A$ and a magnetic field induced by the electric current of the range of $0.02\ T$ [3].

Several studies are available in the literature on the flows in the electrolysis cell. Mathematical models are developed to investigate several impacts of velocity fields on its operation. The proposed models present flow simulations of the two fluids in three dimensions, where different physical phenomena are considered. Various works are carried out for the study of the generation of the bubbles in the electrolytic bath and the two-phase flow of the liquid and the gases [8-13]. Other studies have focused on the impact of flow on the dissolution of alumina in the bath [14]. The interface between the liquid aluminium and the electrolytic bath can be studied using 3D flow models [15, 16]. Simulations of the flow are also done in order to study and test the design of new cells [17-19] or for the study of its thermal balance [5, 20].

Mathematical modeling of 3D flows typically requires the use of turbulence models that take into account fluctuations in velocity over time and space. All the works cited above took into account a turbulence model in order to calculate the velocity field. However, very little information is available on the chosen model over another. In engineering, there are many different approaches for calculating turbulence for different applications [21]. The literature describes many case studies and validation scenarios of turbulence models in different applications, but very few are referring to the case of the electrolysis cell.

This work consists of the modeling of the flow of the fluids in the cell with a particular attention on the turbulence model to represent the velocity field fluctuations during electrolysis operations. The flow model is developed with the basic equations that govern the movement of fluids. Two approaches to represent turbulence are described and used in numerical simulations in order to compare the results. The two models to compare are Large Eddy Simulation (LES) and Reynolds Average Navier-Stokes (RANS). The comparison is made in order to see the viability of the two models to treat turbulence in the electrolysis cell. The hydrodynamic flow is modeled by using simplified conditions, but it is able to reproduce measured turbulence in the cell.

At the end, an attempt is made to compare the numerical results with some in-situ measurements made in an industrial electrolysis cell during its operation. The fluctuation of velocity over time was measured using the principle of drag force due to the flow of liquid aluminium around a body submerged in the aluminium layer.

2. Methods and Mathematical Model Description

The resolution of the equations governing the fluids is quite easily achievable according to numerical schemes available in the literature and such schemes are available in specialized CFD commercial codes. Large velocity fluctuations in the fluids are treated by the way of turbulence models in different industrial applications. Validation must be carried out in order to compare

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6. References

- 1 Halvor Kvande, 3 Production of primary aluminium, Fundamentals of Aluminium Metallurgy, R. Lumley, Ed., 49-69: Woodhead Publishing, 2011.
- 2 François Charmier, Olivier Martin and Réné Gariépy, Development of the AP Technology Through Time, JOM, Vol. 67, no. 2, February 2015, 336-341.
- 3 Alton T. Tabereaux, and Ray D. Peterson, Chapter 2.5 Aluminum Production, Treatise on Process Metallurgy, S. Seetharaman, Ed., Boston: Elsevier, 2014, 839-917.
- 4 S. R. Jakobsen et al., Estimating Alumina Concentration Distribution in Aluminium Electrolysis Cells, IFAC Proceedings Volumes, Vol. 34, No. 18, (2001), 303-308.
- 5 Dagoberto S. Severo, and Vanderlei Gusberti, A modelling approach to estimate bath and metal heat transfer coefficients, Light Metals 2009, 557-562.
- 6 Valdis Bojarevics, and Jim W. Evans, Mathematical modelling of Hall-Héroult pot instability and verification by measurements of anode current distribution, Light Metals 2015, 783-788.
- 7 Joakim Haraldsson, and Maria T. Johansson, Review of measures for improved energy efficiency in production-related processes in the aluminium industry – From electrolysis to recycling, Renewable and Sustainable Energy Reviews, Vol. 93, (2018), 525-548.
- Knut Bech et al., Coupled current distribution and convection simulator for electrolysis cells, Essential Readings in Light Metals: Aluminum Reduction Technology, Volume 2, 2013, 396-401 (from Light Metals 2001, 463).
- 9 Kristian Etienne Einarsrud, Stein Tore Johansen and Ingo Eick, Anodic bubble behaviour in Hall-Héroult cells, Light Metals 2012, 875-880.
- 10 Zhiming Liu et al., Current efficiency predictive model and its calibration and validation, Light Metals 2012, 935-938, 2012.
- 11 Dagoberto S. Severo et al., Modeling the bubble driven flow in the electrolyte as a tool for slotted anode design improvement, Essential Readings in Light Metals: Aluminum Reduction Technology, Volume 2, 409-414, 2013 (from Light Metals 2007, 287-292).
- 12 Shuiqing Zhan et al., A CFD- PBM coupled model predicting anodic bubble size distribution in aluminum reduction cells, Light Metals 2014, 777-782.
- 13 Yiwen Zhou et al., Simulation of Anode Bubble: Volume of Fluid Method, Light Metals 2014, 783-788.
- 14 Yuqing Feng, Mark A. Cooksey, M. Philip Schwarz, CFD modelling of alumina mixing in aluminium reduction cells, Light Metals 2010, 543-548.
- 15 Jinsong Hua et al., Revised benchmark problem for modeling of metal flow and metal heaving in reduction cells, Light Metals 2014, 691-695.
- 16 Dagoberto S. Severo et al., "Comparison of various methods for modeling the metalbath interface," Essential Readings in Light Metals: Aluminum Reduction Technology, Volume 2, 2013, 379-384 (from Light Metals 2008, 413-418).
- 17 Amit Gupta et al., Electromagnetic and MHD study to improve cell performance of an end- to- end 86 kA potline, Light Metals 2012, 853-858.

- 18 Zhiming Liu, Fengqin Liu, Yueyong Wang, Flow field comparison between traditional cell and new structure cell by CHALCO by CFD method, Light Metals 2012, 955-958.
- 19 Qiang Wang et al., Effect of innovative cathode on bath/metal interface fluctuation in aluminum electrolytic cell, Light Metals 2014, 491-494.
- 20 Kristian Etienne Einarsrud, Egil Skybakmoen, Asbjørn Solheim, On the influence of MHD driven convection on cathode wear, Light Metals 2014, 485-490.
- 21 Wolfgang Rodi, Turbulence models and their application in hydraulics, Routledge, 2017.
- 22 Dagoberto S. Severo et al., Modeling magnetohydrodynamics of aluminum electrolysis cells with ANSYS and CFX, Light Metals 2005, 475-480.
- 23 CFX-ANSYS, Release 11.0. Ansys CFX-Solver modeling Guide, ANSYS, Inc., 2009.
- 24 CFX-Solver-ANSYS, Theory Guide, Release II, 2006.
- 25 Brian E. Launder, and D. Brian Spalding, The numerical computation of turbulent flows, Computer Methods in Applied Mechanics and Engineering, Vol. 3, No. 2, (1974), 269-289.
- 26 M. Lateb et al., Comparison of various types of k–ε models for pollutant emissions around a two-building configuration, Journal of Wind Engineering and Industrial Aerodynamics, Vol. 115, April 2013, 9-21.
- J. Smagorinsky, General circulation experiments with the primitive equations: I. The basic experiment, Monthly Weather Review, Vol. 91, No. 3, (1963), 99-164.
- 28 M. Rieth et al., Comparison of the Sigma and Smagorinsky LES models for grid generated turbulence and a channel flow," Computers & Fluids, Vol. 99, 22 July 2014, 172-181.
- 29 R. Hernández-Walls et al., Design and calibration of an inexpensive digital anemometer, Physics Education, Vol. 43, No. 6, 2008, 593.
- 30 A. Moros, Drag anemometry for measuring velocities in electromagnetically driven flows, Journal of Physics E: Scientific Instruments, Vol. 19, No. 12, (1986), 1050.
- 31 C. Hopley, and M. Tunstall, A fast response anemometer for measuring the turbulence characteristics of the natural wind, Journal of Physics E: Scientific Instruments, Vol. 4, No. 7, 1971, 489.
- 32 A. Green et al., A rapid-response 2-D drag anemometer for atmospheric turbulence measurements, Boundary-Layer Meteorology, Vol. 57, No. 1-2, (1991), 1-15.
- 33 Samaneh Poursaman, Development of a drag probe for in-situ velocity measurement of molten aluminum in electrolysis cell, Master Thesis, Civil and Water Engineering Department, Laval University, 2018.
- 34 Mounir Baiteche *et al.*, "LES turbulence modeling approach for molten aluminium and electrolyte flow in aluminum electrolysis cell," *Light Metals 2017*, pp. 679-686: Springer, 2017.