

Properties of Lithium Modified Baths for Hall-Héroult Cells

Asbjørn Solheim

Chief Scientist

SINTEF Materials and Chemistry, Trondheim, Norway

Corresponding author: asbjorn.solheim@sintef.no

Abstract



Some aspects concerning the use of lithium-modified baths in aluminium electrolysis cells were considered. Based on literature data, a number of physical and chemical properties were calculated for two cases: i) the bath composition was assumed to follow a liquidus temperature isotherm by adding lithium while at the same time reducing the amount of excess aluminium fluoride, or: ii) the bath was modified by adding lithium fluoride while keeping the amount of excess aluminium fluoride constant. Compared with normal bath compositions, lithium modified baths have higher electrical conductivity, lower alumina solubility, lower vapour pressure, higher density, higher viscosity, and higher surface tension. The current efficiency decreases when the composition follows a liquidus isotherm, but increases when lithium fluoride is added at constant aluminium fluoride. The main way for lithium out of the process is with produced bath. Using alumina containing 0.4 wt% sodium oxide and 0.04 wt% calcium oxide, the stationary consumption of lithium carbonate was estimated to be 0.32 kg/t Al.

Keywords: Electrolyte; lithium fluoride; physical data; current efficiency.

1. Introduction

The use of lithium fluoride (LiF) modified bath in aluminium electrolysis cells was more common a few decades ago. Until about 1970 - 1980, baths with only 5 wt% excess aluminium fluoride (AlF_3) were standard, and temperatures around 980 °C was considered normal. The temperature can be reduced by any fluoride, but adding more AlF_3 , LiF, magnesium fluoride (MgF_2), or a combination of those have been considered to be the best options. The main benefit with LiF is the strongly increased electrical conductivity. Some of the older literature also refers to increased current efficiency (CE), while newer data indicate that the CE will be constant or reduced.

Pechiney changed the bath composition in the acid direction (more excess AlF_3) in 1978. Trials with LiF modified bath in 180 kA cells were performed in the 1980s, but these tests were not pursued [1]. Some tests were also performed in Pechiney's 280 kA cells some years later [2], but also in this case, it was found that the use of LiF was not profitable. Venalum used LiF-modified bath in the 1980s. After the introduction of point feeders, the composition was changed in the acid direction without LiF [3, 4].

Although the use of lithium modified bath is not a hot topic today, it is an idea that is being reconsidered from time to time. In the few cases where addition of LiF has been tried in modern cells [5, 6], the motivation has been to increase the amperage, to obtain better stability by increasing the anode-cathode distance (ACD), or to reduce the specific energy consumption (in spite of slightly reduced current efficiency). According to Tabereaux *et al.* [5] the optimum LiF concentration may be about 1 wt%.

The purpose of the present work is to quantify and illustrate the consequences of introducing LiF in modern cells. The author does not intend to give specific advice or recommendations concerning the use of LiF-modified bath. Hopefully, the data and considerations presented here may be helpful during the first part of a decision process concerning bath modification.

2. Bath Modification Paths

Bath modification can take place along two paths: i) by replacing AlF_3 by LiF in such a way that the liquidus temperature remains constant, or: ii) by simply adding LiF while keeping the excess AlF_3 constant (all combinations of these paths are, of course, possible). The paths are illustrated in Figure 1. The liquidus isotherms were calculated from the equation by Solheim *et al.* [7], from which 3°C was subtracted to account for impurity elements. It is noteworthy that when one starts at 955°C liquidus temperature, not much more than 2 wt% LiF can be added without reducing the liquidus temperature.

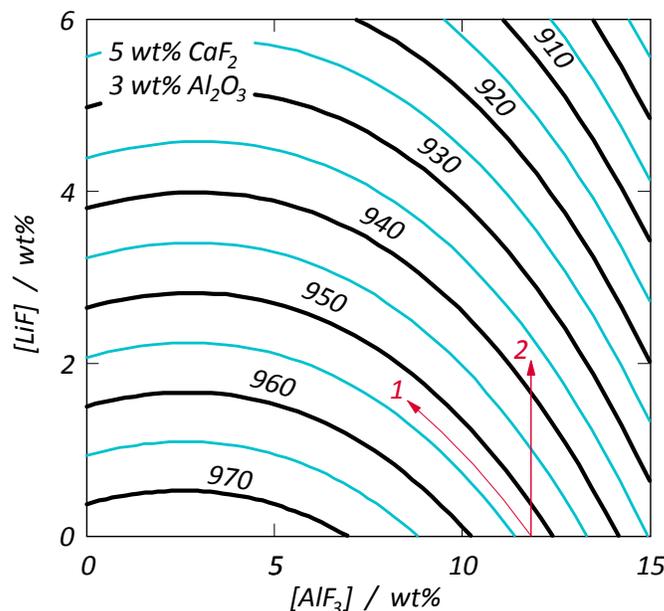


Figure 1. Liquidus isotherms for the system Na_3AlF_6 -5 wt% CaF_2 -3 wt% Al_2O_3 - AlF_3 -LiF [7]. Path 1: Constant liquidus temperature, Path 2: constant excess AlF_3 (see the text).

3. Some Physical and Chemical Properties

The figures in this section show different physical and chemical properties as a function of the concentration of LiF. The bath composition was supposed to follow the two paths shown in Figure 1. In all cases, the superheat was assumed to be 10°C , and the bath always contains 5 wt% CaF_2 and 3 wt% Al_2O_3 . The data obtained with Path 1 (constant liquidus temperature) show "hooks" at the end of the curves, which is related to the fact that the liquidus isotherms pass through maxima.

3.1. Electrical conductivity

Increased electrical conductivity is the strongest motivation for introducing LiF modified bath. The electrical conductivity was calculated from the equation suggested by Hives *et al.* [8], and the result

8. References

1. M. Keinborg and J.P. Cuny: Aluminium Pechiney 180 kA Prebake Pot from Prototype to Potline, *Light Metals 1982*, 449-460.
2. B. Langon and P. Varin: Aluminium Pechiney 280 kA Pots, *Light Metals 1986*, 343-347.
3. F. Mosquera and H. Medina: The Optimum Bath Ratio in Modified Baths, *Light Metals 1987*, 303-307.
4. H. Medina and N. Elarba: Modernization of Venalum Pots to Meet New Requirements and Higher Performance, *Light Metals 1988*, 623-626.
5. A.T. Tabereaux, T.R. Alcorn, and L. Trembley: Lithium-modified Low Ratio Electrolyte Chemistry for Improved Performance in Modern Reduction Cells, *Light Metals 1993*, 221-232.
6. S. Stejer, B. Hullett, and N. Urata: Application of Lithium Modified Electrolyte in High Current Density Aluminium Reduction Cells, *Light Metals 2001*, 199-206.
7. A. Solheim, S. Rolseth, E. Skybakmoen, L. Støen, Å. Sterten, and T. Støre: Liquidus Temperatures for Primary Crystallization of Cryolite in Molten Salt Systems of Interest for the Aluminium Electrolysis, *Met. Mater. Trans. B* 27 B (1996), 739-744.
8. J. Hives, J. Thonstad, Å. Sterten, and P. Fellner: Electrical Conductivity of Molten Cryolite-based Mixtures Obtained with a Tube-type Cell Made of Pyrolytic Boron Nitride, *Met. Mater. Trans. B*, 27B (2), (1996), 255-261.
9. E. Skybakmoen, A. Solheim, and Å. Sterten: Alumina Solubility in Molten Salt Systems of Interest for Aluminium Electrolysis and Related Phase Diagram Data, *Met. Trans. B*, 28B (1997), 81-86.
10. A. Solheim: The Density of Molten NaF-LiF-AlF₃-CaF₂-Al₂O₃ in Aluminium Electrolysis, *Aluminium Transactions*, 2 (1) (2000), 161-168.
11. W.E. Haupin and H. Kvande: Mathematical Model of Fluoride Evolution from Hall-Heroult Cells, *Light Metals 1993*, 257-263.
12. T. Herzberg, K. Tørklep, and H.A. Øye: Viscosity of Molten NaF-AlF₃-Al₂O₃-CaF₂ Mixtures. Selecting and Fitting Models in a Complex System, *Light Metals 1980*, 159-170.
13. M. Chrenkova, V. Danek, A. Silny, and T. Utigard: Density, Electrical Conductivity and Viscosity of Low Melting Baths in Aluminium Electrolysis, *Light Metals 1996*, 227-232.
14. V. Danek, O. Patarak, and T. Østvold: Surface Tension of Cryolite-based Melts, *Can. Metall. Quart.*, 34 (2) (1995), 129-133.
15. A. Solheim, H. Gudbrandsen, K.S. Osen, and J. Kvello: Current Efficiency in Laboratory Aluminium Cells, *Proceedings of 33rd International ICSOBA Conference, Travaux No. 44*, Dubai, United Arab Emirates, 29 November-1 December 2015, Paper AL14, 625-634.
16. R.D. Peterson and A.T. Tabereaux: Effect of Bath Additives on Aluminum Metal Purity, *Light Metals 1986*, 491-499.
17. K. Mizoguchi and K. Yuhki: Appraisal of the Operation of Horizontal-stud Cells with the Addition of Lithium Fluoride, *Light Metals 1971*, 175-187.
18. G. Kuschel and B.J. Welch: Lithium Losses During Addition and Dissolution of Various Forms of Lithium Carbonate to Electrolytes, *Light Metals 1986*, 445-449.
19. NIST-JANAF Thermochemical Tables, <http://kinetics.nist.gov/janaf/>
20. R.D. Peterson and A.T. Tabereaux: Lithium Fluoride Losses from Cryolitic Baths in Hall-Heroult Cells, *Light Metals 1988*, 647-654.